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The Private Securities Litigation Reform Act of 1995 provides a "safe harbor" for certain forward-looking statements so long as such information is identified as forward-looking and is accompanied by meaningful cautionary statements identifying important factors that could cause actual results to differ materially from those projected in the information.

The use of words such as "may", "might", "will", "should", "expect", "plan", "outlook", "anticipate", "believe", "estimate", "appear", "project", "intend", "future", "potential" or "continue", and other similar expressions are intended to identify forward-looking statements.

All of these forward-looking statements are based on estimates and assumptions by our management that, although we believe to be reasonable, are inherently uncertain. Forward-looking statements involve risks and uncertainties, including, but not limited to, economic, competitive, governmental and technological factors outside of our control, that may cause our business, industry, strategy or actual results to differ materially from the forward-looking statements.

These risks and uncertainties may include those discussed in the Company's most recent filings with the Securities and Exchange Commission, and other factors which may not be known to us. Any forward-looking statement speaks only as of its date. We undertake no obligation to publicly update or revise any forward-looking statement, whether as a result of new information, future events or otherwise, except as required by law.

Confidentiality

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- LNG is safer than Propane
- A pressurized tank of LNG will NOT explode
- LNG will not ignite or burn, the mixture is too rich
- LNG vapor will only ignite in concentrations between 5 to 15%
- If there is an LNG leak, control the vapor cloud with a water wall to direct the vapor cloud away from any ignition source
- DO NOT put water directly on or into an LNG leak

LNGoTM SYSTEM OVERVIEW

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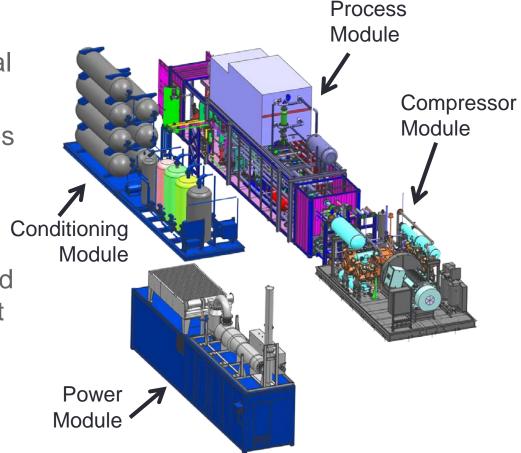
LNGo[™] System Overview

 Modular and portable natural gas liquefaction plant is:

Comprised of four modules

 Capable of producing 6,000 gallons of LNG per day

 Designed for over-the-road shipment to be installed at the natural gas source



CONFIGURATION FOR MARKETS WITH PIPELINE QUALITY GAS INPUT AT 35 PSIGSHOWN

Process consumes: ~3.12 kW-h/gal (~1.95 kW-h/kg) LNG

CONDITIONING MODULE—

Molecular sieve removes CO_2 and H_2O . The purge flow, with C_2 and above, is blended into the fuel supply to the <u>Guascor</u>[®] engine

POWER MODULE—Genset driven by <u>Guascor</u>® 1MW engine consumes purge gas from mole sieve to power unit

Enginuity® Control and Monitoring Systems

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PROCESS MODULE—delivers 6,000 gallons (~9.6 tonnes) LNG per day

COMPRESSOR MODULE— <u>MOS</u>™ Compressor drives efficient process

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Product Specifications

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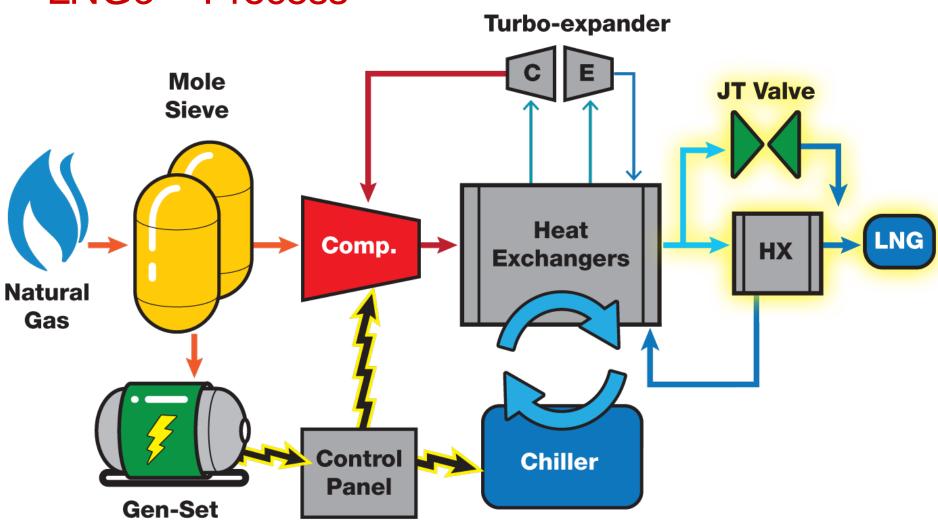
LNGo[™] Product Specifications

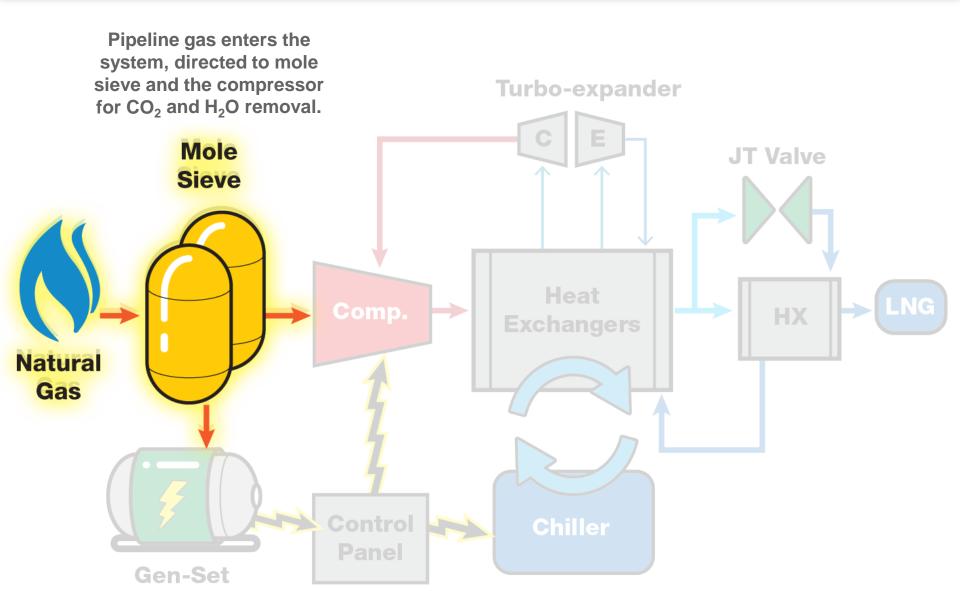
- Meets NEC Class 1, Division 2, Group D, T2A for areas certified as hazardous
- Ambient Rating: -40°F to 110°F
- Module Assembled Footprint: 110' x 50' x 14' (h)
- Input Natural Gas:
 - 707 MSCFD (Thousand Standard Cubic Feet per Day)
 - Nominal inlet condition 35 psig, 60°F
- Output LNG:
 - 6000 gallons per day (GPD)
 - 10-85 psig
 - -252°F

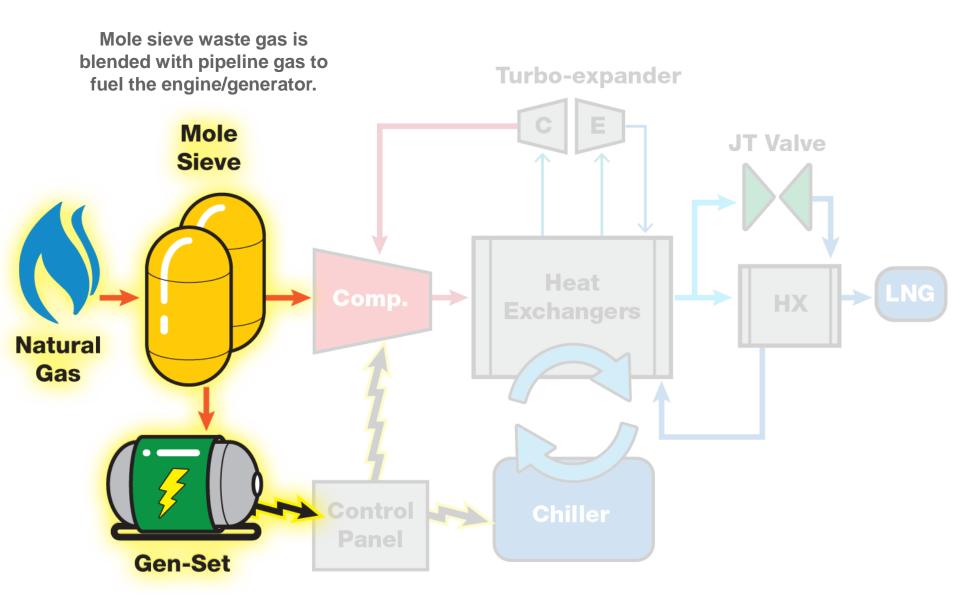
LNGoTM Process

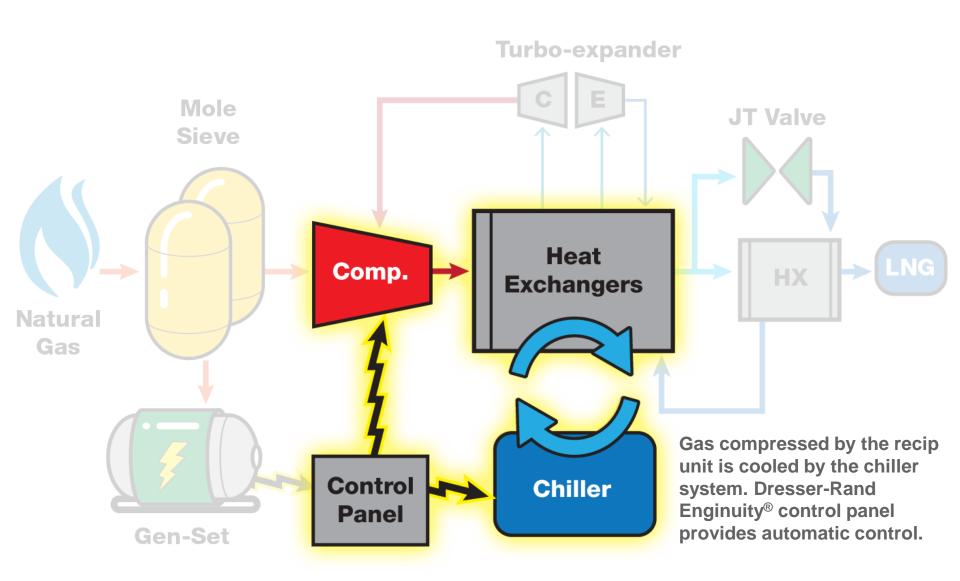
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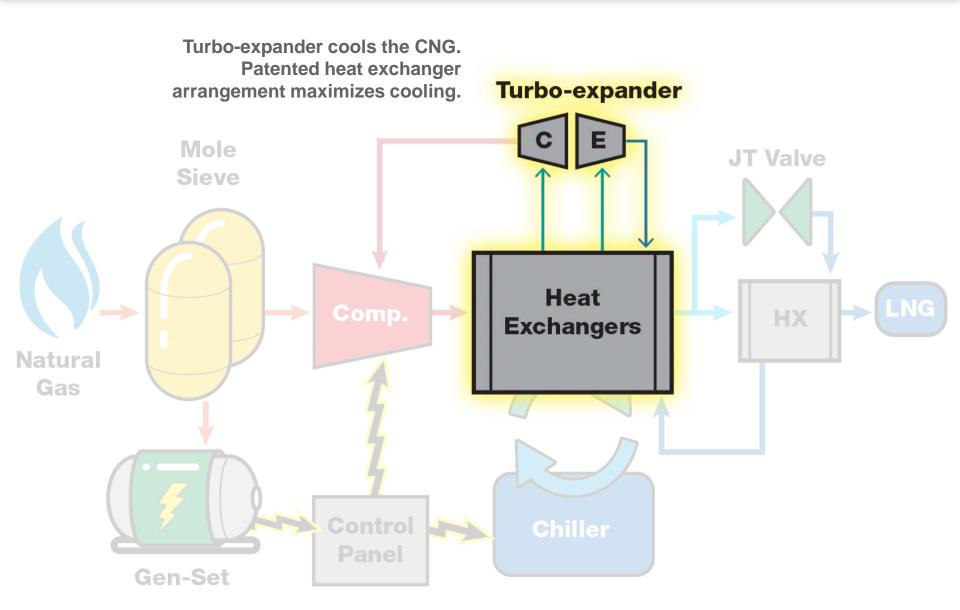
LNGoTM Process

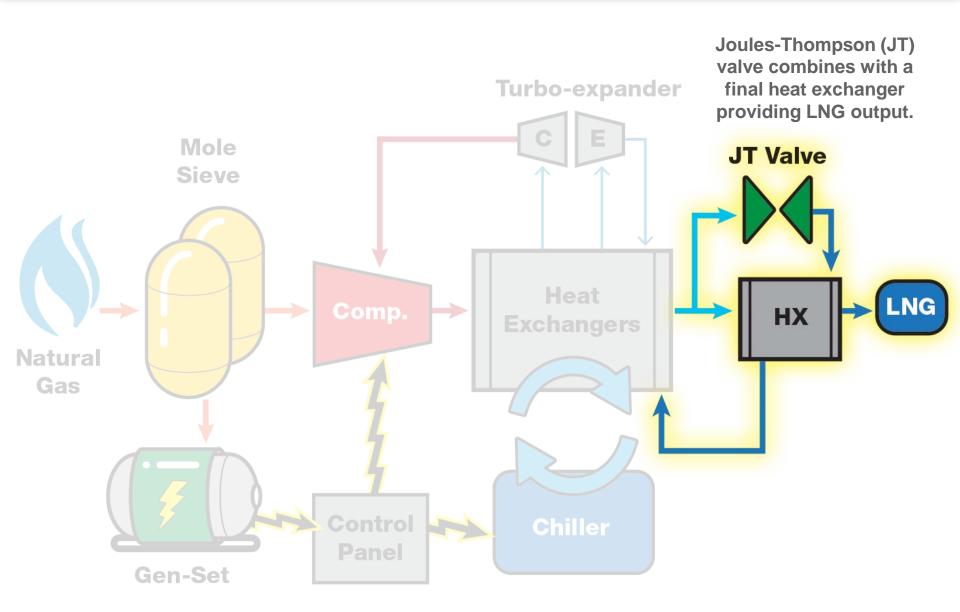












System Configuration

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Power Module

Provides electrical power for the entire LNGo™ system

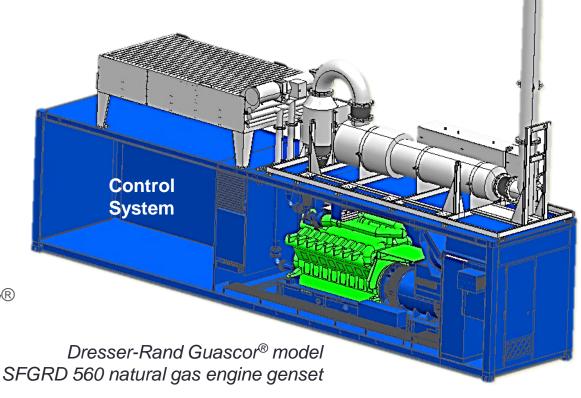
Engine configured to handle natural gas within an LHV range of 800

to 1150 BTU/CF

 Fuel gas is a blended mixture of Mole
 Sieve purge (waste) gas and inlet NG

 Guascor: 16-cylinder, 4 cycle, turbocharged and after cooled richburn engine

Dresser-Rand Enginuity[®]
 Control System



Power Module

- Rated emissions of 0.1/0.2/0.2 gm/bhp-hr for NOx/CO/NMHC
- Genset package is rated for 870 kW at 1800 RPM
- Fan-driven ambient air cooler to cool engine jacket and lube oil circuits
- Contains a PLC based LNGoTM control system
- Contains motor control center (MCC)





Conditioning Module

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The conditioning module, also known as a molecular sieve, takes the incoming gas and cleans and separates it into two streams

The product stream, now free of H₂O or CO₂, is fed to the MOS[™] compressor to begin the liquefaction process

The purge stream is essentially a waste stream that contains H₂O, CO₂ and heavier hydrocarbons that are not permissible for making LNG. The purge stream is blended with make-up natural gas and consumed to fuel the Guascor® engine, avoiding additional gas treatment or cleanup

Conditioning Module

- Flow meters to measure the gas flow from Purge and Product streams
- 75 HP electric motor driven vacuum compressor to pull the tail gas stream from the regenerating vessel



- Three pressure swing adsorption (PSA) vessels that contain the adsorbent media for the molecular sieve
- Depressurization and re-pressurization tanks to smooth out pressure fluctuation between cycles
- A series of pneumatic actuated control valves for directing gas flow from regenerating vessel to storage tank



Compressor Module

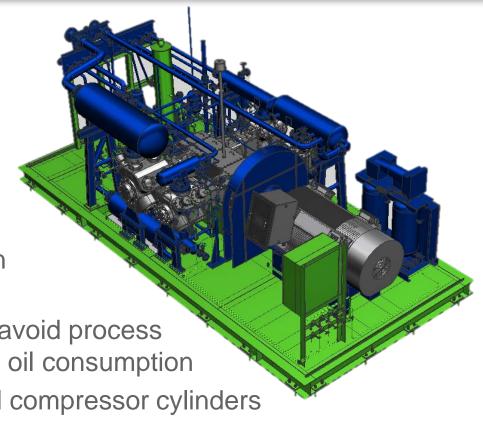
Satisfies all four stages of gas compression required by the LNGo[™] liquefaction system

Dresser-Rand Model 7MOS4
 Reciprocating Compressor driven
 by VFD powered electric motor

 Uses non-lubricated cylinders to avoid process contamination and eliminate lube oil consumption

 Water-glycol coolant used to cool compressor cylinders and rod packings

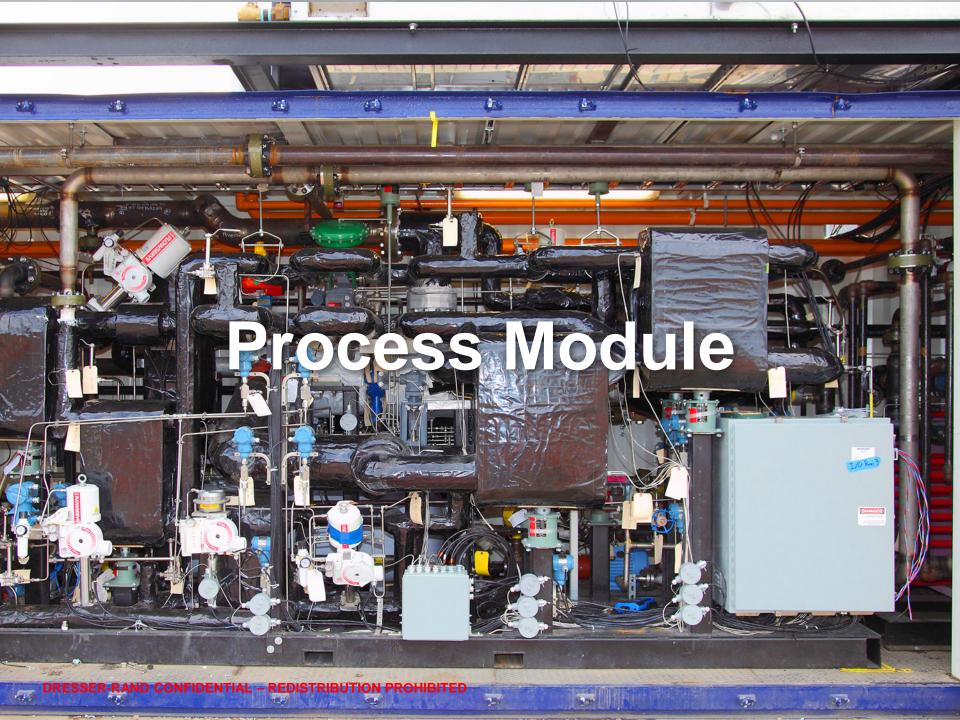
 Crankshaft and rod bearings lube oil fed by a mechanically driven pump during normal operation and electric motor-pump during startup



Compressor Module

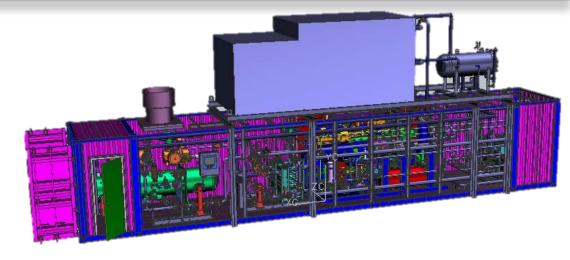
- Includes lube oil & water/glycol coolant console with electric motors/pumps to supply coolant pressure during startup and shut down
- Features Magnum[®] XF series valves for proven combination of efficiency and durability in high pressure ratio applications
- Induction drive motor rated at 550 HP at 480V, 60 Hz, 3 phase power
- Includes variable frequency drive with harmonic filter





Process Module

Contains liquefaction process piping and heat exchangers required to drop the pressure and



reduce the temperature of the natural gas

- Turbo-expander seal gas system delivers buffer natural gas to seal the bearing housing against process pressures and temperatures
- Anti-surge control system protects the turbo-expander against surge by recycling gas from the compressor discharge
- Stainless steel cryogenic heat exchangers fabricated from brazed steel plates
- Mechanical chiller uses ammonia refrigeration loop cooled by evaporative cooling

Process Module

- Mechanical Chiller (1st phase of cooling)
 - Supplies the process heat exchangers with ammonia chilling
 - Reduces temperature of ammonia through an evaporative cooler
- Turbo-Expander (2nd phase of cooling)
 - Reduces the temperature by expanding the natural gas
 - Supplies the cryogenic heat exchangers with gas refrigeration
 - Compressor and expander wheels connected by common shaft inside a horizontally split case
 - Expander wheel uses variable inlet guide vanes to control inlet gas flow and maximize efficiency
- Joules Thompson Valve (Final subcooling)
 - Rapidly expands natural gas and reduces temperature to below -250F
 - Used to supply final cryogenic heat exchanger with cooling medium



Values and Features

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LNGo[™] Values and Features

- Value Proposition
 - Re-deployable
 - Premier, proven D-R engineered product technologies
 - Shortest cycle time (less than 6 months from order to operation)
 - Worldwide service and support
 - Inventory available NOW!
- LNGo Features
 - Skid-mounted design and small footprint
 - 6000 gpd—perfect size for local LNG production and demand
 - Multi-market applications
 - Self-powered (requiring no external utilities)
 - Easy to permit (no flaring required)



Controls, Monitoring and Safety Systems

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Controls, Monitoring and Safety Systems

- Contains PLC based control panel that controls and monitors entire system via HMI located in control room
- Equipped with condition monitoring system for remote access to performance data
- Combustible gas detection to monitor accumulation of vapors
- Low temperature detectors to detect LNG spill
- Fire detection by using smoke, high temperature, and UV/IR flame detectors
- Automatic alarm and shutdowns protect process safety under abnormal operating conditions



Codes/Standards

The following codes and standards may have application to the design and testing of the LNGo 6,000 gpd distributed LNG Production Plant

49 CFR Part 193 -2012—Liquefied Natural Gas Facilities Federal Safety Standards

Edition

23 CFR 658, PERM30(NY)—Truck Size and weight, Route Designations — Length, Width and Weight Limitations NFPA 59A—Standard for the Production, Storage and Handling of Liquefied Natural Gas (LNG), 2013 Edition NFPA 30—Flammable and Combustible Liquids Code. 2012

NFPA 70–National Electric Code, 2013 Edition NFPA 56(PS) –Standard Fire and Explosion Prevention During Cleaning and Purging of Flammable Gas Piping Systems, 2012 Edition

ASME B31.3—Process Piping, 2012 Edition
ASME Sect VIII—Boiler and Pressure Vessel Codes, 2012
Edition

CGA S-1.3—Pressure Relief Device Standards, Part 3 — Stationary Storage Containers for Compressed Gases, 2008, 8'th Edition

AGA-Purging Principles and Practice
ASTM A105/A105M-12 Standard Specification for Carbon
Steel Forgings for Piping Applications
ASTM A312 / A312M-12a Standard Specification for
Seamless, Welded, and Heavily Cold Worked Austenitic SS
Pipes

ASTM A182 / A182M–13 Standard Specification for Forged or Rolled Alloy and Stainless Steel Pipe Flanges, Forged Fittings, and Valves and Parts for High-Temperature Svc.

API 520–Reciprocating Compressors for Petroleum, Chemical, and Gas Industry Services, Eighth Edition, 2008.

API 526–Flanged Steel Pressure Relief Valves, Fifth Edition 2002

API 527—Seat Tightness of Pressure Relief Valves, Third Edition, R(2002)

API 598–Valve Inspection and Testing. Ninth Edition, 2009. API 614–Lubrication, Shaft Sealing, and Oil-control Systems and Auxiliaries, 5'th Edition, 2008, as applicable.

API 617—Axial and Centrifugal Compressors and Expandercompressors for Petroleum, Chemical and Gas Industry Services, Seventh Edition, 2002.

API 618–Reciprocating Compressors for Petroleum, Chemical, and Gas Industry Services, Fifth Edition, 2007. The separable unit is not API 618, however, principles of 618 apply.

API 670–Machinery Protection Systems, Fourth Edition 2010.

API 688—Pulsations and Vibration Control in Positive Displacement Machinery Systems for Petroleum, Petrochemical, and Natural Gas Services, Guideline only First Edition 2012.



Documentation Submittal (typical)

LNGo[™] DOCUMENTATION SUBMITTAL LISTING:

- LNGo™ Site Plan
- General Arrangement: Compressor Module
- General Arrangement:
 Process Module
- General Arrangement:
 Power Module
- General Arrangement: Conditioning Module
- Lifting and Shipping Plan
- P&ID: LNGoTM Process
- Interconnecting Diagram
- Inspection and Test Plan
- Inspection Report/s

PRELIMINARY TECHNICAL MANUAL

LN*Go*TM Technical Manual includes P&IDs, Bills of Material, Assembly Drawings, Technical Data for:

- LNGoTM Auxiliary Systems
- Process Gas
- Reciprocating Compressor Oil
- Reciprocating Compressor Coolant
- Control Air
- Engine
- Molecular Sieve
- Chiller System
- Control Air
- Motor
- Oil/water Console



Thank You

